WO 2005/009939 PCT/GB2004/002686

Claims

10

- 1. A catalyst system for the production of acetic acid which catalyst system comprises an iridium carbonylation catalyst, methyl iodide co-catalyst, optionally at least one of ruthenium, osmium, rhenium, zinc, gallium, tungsten, cadmium, mercury and indium and at least one non-hydrohalogenoic acid promoter.
- 5 2. A catalyst system according to claim 1 wherein the non-hydrohalogenoic acid is selected from an oxoacid, a superacid, a heteropolyacid and mixtures thereof.
 - 3. A catalyst system according to claim 2 wherein the non-hydrohalogenoic acid is an oxoacid.
 - 4. A catalyst system according to claim 3 wherein the oxoacid is an oxoacid of the elements of Groups 13 to 17 of the Periodic Table.
 - 5. A catalyst system according to claim 3 or claim 4 wherein the oxoacid is selected from H₂SO₄, HNO₃, H₃PO₄ and mixtures thereof.
 - 6. A catalyst system according to any one of claims 3 to 5 wherein the molar ratio of oxoacid anion to iridium is in the range [greater than 0 to 0.4]: 1.
- 7. A catalyst system according to claim 5 wherein the molar ratio of oxoacid anion to iridium is [greater than 0 to 0.35]: 1, such as in the range [0.05 to 0.3]: 1.
 - 8. A catalyst system according to claim 2 wherein the non-hydrohalogenoic acid is a superacid.
- 9. A catalyst system according to claim 8 wherein the superacid has a non-20 coordinating anion to iridium.
 - 10. A catalyst system according to claim 8 or claim 9 wherein the superacid is a superacid having an anion selected from BF₄, PF₆, (CF₃SO₂)₂N, CBH₆Br₆, CF₃SO₃, SbF₆, FSO₃ and mixtures thereof.

WO 2005/009939 PCT/GB2004/002686

11. A catalyst system according to any one of claims 8 to 10 wherein the superacid is selected from HBF₄, HPF₆, (CF₃SO₂)₂NH, HCBH₆Br₆ and mixtures thereof.

- 12. A catalyst system according to any one of claims 8 to 11 wherein the molar ratio of the superacid anion to iridium is in the range [greater than 0 to 2.5]: 1.
- 5 13. A catalyst system according to claim 12 wherein the molar ratio of the superacid anion to iridium is in the range [greater than 0 to 1]: 1, such as in the range [0.05 to 0.5]: 1.
 - 14. A catalyst system according to claim 2 wherein the non-hydrohalogenoic acid is a heteropolyacid.
- 10 15. A catalyst system according to claim 14 wherein the heteropolyacid comprises molybdenum and/or tungsten as peripheral atoms.
 - 16. A catalyst system according to claim 15 wherein the heteropolyacid is selected from 12-tungstophosphoric acid, 12-molybdophosphoric acid, 12-tungstosilicic acid, 12-molybdosilicic acid and mixtures thereof.
- 17. A catalyst system according to any one of claims 14 to 16 wherein the molar ratio of the heteropolyacid anion to iridium is in the range [greater than 0 to 5]: 1.
 - 18. A catalyst system according to claim 17 wherein the molar ratio of the heteropolyacid anion to iridium is in the range [greater than 1 to 4]:1, such as in the range [1.5 to 3.5]:1.
- 20 19. A catalyst system according to any one of claims 1 to 18 which comprises at least one of ruthenium, osmium, rhenium, zinc, gallium, tungsten, cadmium, mercury and indium.
 - 20. A catalyst system according to claim 19 which comprises at least one of ruthenium, osmium, rhenium and indium.
- 21. A process for the production of acetic acid by reacting carbon monoxide with methanol and/or a reactive derivative thereof in a liquid reaction composition comprising methyl acetate, a finite concentration of water, acetic acid and a catalyst system comprising a catalyst system according to any one of claims 1 to 20.

30

- 22. A process according to claim 21 wherein the concentration of methyl acetate in the liquid reaction composition is in the range 1 to 70% by weight.
- 23. A process according to claim 22 wherein the methyl acetate concentration is in the range 2 to 50% by weight, such as 3 to 35% by weight.
- 24. A process according to any one of claims 21 to 23 wherein the concentration of